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## Numerical investigation of Hydro-magnetic flow of air in three different geometries of open cavity Payam Fadaei<sup>1</sup>, Mohamad Hassan Djavareshkian<sup>2</sup>, Amir Javad Ahrar<sup>3,\*</sup>

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### Abstract

MHD or Magnetic hydro dynamics of an open cavity with three different depths is investigated numerically in this paper. The SIMPLE algorithm is utilized in order to solve the equations of conservation of momentum and energy. Isothermal lines and streamlines of the flow are presented for 3 Ha numbers: Ha=10, 20, and 30 for each of the three cavity depths: L, 2L, and 3L. Then the Nu number of the heated wall has been studied and compared for each Ha number and cavity depth. It was observed that in the case of depth L and Ha=30 the maximum heat transfer is achieved while the minimum heat transfer rate is for the case of depth 2L and Ha=20.

Keywords: MHD, open cavity, mixed convection

### Introduction

Generally, cavities can be classified into two major groups; namely closed and open cavities. The open cavities' heat transfer and mass flow have been investigated widely due to their significant applications in many industries such as: solar concentrators, lakes and reservoirs, refrigeration, cooling process of electric devices and fire researches [1-5]. Also, the problems of natural convection and hydro magnetic flow have been major topics of research during the last decade. Their wide occurrence in many industrial cases like: crystal growth, oil extraction, electronic cooling and solar collectors make them undeniable [6-9].

In 1992, Braga and Viskanta [10] reported an experimental and theoretical investigation of transient natural convection in a rectangular cavity. Al-Nimr obtained analytical solutions for MHD fully developed upward (heating) or downward (cooling) natural convection in open ended porous annuli (1995) [11]. Later on in 1999, Al-Nimr and Hader modified their solution for more general thermal boundary conditions [12].

Ishikawa et al. (2000) numerically investigated the natural convection with density inversion in a square cavity with variable fluid properties [13]. Hossain and Rees in 2005 studied unsteady laminar natural convection flow of water in a rectangular cavity and found that the heat generation rate and the mean temperature of solid walls play an important role in the flow and temperature fields [14]. Kandaswamy et al. [15] investigated the heat transfer rate of partially active walls of a square cavity. They found that the

heat transfer rate is maximum for middle – middle thermally active location and it is very poor for the top – bottom locations (2008).

In 2011, Sivasankaran et al. numerically investigated the magneto-convection of cold water in an open cavity with variable fluid properties. In their work it was observed that the convection heat transfer is enhanced by thermo capillary force when buoyancy force is weakened [16]. Oztop et al. made a numerical study on the MHD mixed convection in a lid driven cavity with corner heater. They applied a finite volume technique to observe the fluid flow and temperature fields under different Grashof and Hartmann numbers. They have taken the Joule effect under account in their study [17].

In 2012, the LBM (Lattice Boltzmann Method) method was applied to solve the fluid flow and energy equations. Nemati et al. used LBM to study the Magnetic field effects on natural convection flow of nanofluid in a rectangular cavity. They found that the average Nusselt number increases for nanofluid when increasing the solid volume fraction, while, in the presence of a strong magnetic field, this effect decreases [18]. Kefayati et al. used the same method to simulate the MHD mixed convection in a lid driven cavity with linearly heated wall [19]. They studied the influence of Richardson and Hartmann Numbers as well as the inclination angle of the magnetic field on the convection heat transfer rate.

Also in this year, Prakash et al. investigated the natural convection of open cavities numerically. Different shapes of open cavities were considered in their work such as: cubical, hemispherical and spherical. They presented the 3D results of the convective loss and Nu number of these cavities [20]. Rahman et al. (2012) have made a computational study on the mixed convection of an open square cavity heated from different sides [21]. They reported their results for fixed Ha and Re numbers. In this work the mixed convection of an open cavity is investigated for different Ha numbers and different cavity depths.

# Geometry and governing equations Studied model geometries

The geometries and boundary conditions which are considered in this work are presented in figure 1(a) - (c). The open cavity includes an open channel from which the flow enters and exits, and a cavity with the depths of L, 2L, and 3L. The length of the channel and the bottom wall of cavity are fixed to 2L and L, respectively. The bottom wall of the cavity is assumed to have a fixed temperature

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of  $T_h$  while all other walls are adiabatic. The flow enters the channel at a uniform velocity of  $U_{in}$  and temperature of  $T_{in}$ . A magnetic field is acting on the *x* direction with variable intensities due to different Ha numbers. Finally, the gravity is acting downward in the vertical direction.

### Governing equations and boundary conditions

The equations of two dimensional steady, incompressible fluid flow were solved numerically. In this work the effects of Joule heating and dissipation were neglected. The dimensionless equations of motion under Boussinesq approximation are as follows:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0$$

$$U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} = -\frac{\partial P}{\partial X} + \frac{1}{\text{Re}} \left( \frac{\partial^2 U}{\partial X^2} + \frac{\partial^2 U}{\partial Y^2} \right)$$

$$U \frac{\partial V}{\partial X} + V \frac{\partial V}{\partial Y} = -\frac{\partial P}{\partial Y} + \frac{1}{\text{Re}} \left( \frac{\partial^2 V}{\partial X^2} + \frac{\partial^2 V}{\partial Y^2} \right) + \frac{Ra}{\text{Re}^2 \text{Pr}} \theta + \frac{Ha^2}{\text{Re}} V$$

$$U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} = \frac{1}{\text{Re} \text{Pr}} \left( \frac{\partial^2 \theta}{\partial X^2} + \frac{\partial^2 \theta}{\partial Y^2} \right)$$

In the above equations the dimensionless numbers are defined as:

$$Re = \frac{u L}{v}, Pr = \frac{v}{\alpha}.$$

$$Ra = \frac{g \beta \neq (T_{-} - T_{-})L^{3}}{v\alpha}, Ha^{2} = \frac{\sigma B_{0}^{2}L^{2}}{\mu}$$

Where the non-dimensionalizing quantities are:

$$X = \frac{x}{L} \quad Y = \frac{y}{L} \qquad U = \frac{u}{u_{in}} \qquad V = \frac{v}{u}$$
$$P = \frac{\left(p + \rho gy\right)L^2}{\rho u_{in}^2} \qquad \Theta = \frac{T - T_{in}}{T_h - T_{in}}$$

The boundary conditions which were considered for this case are as follows:

Inlet: 
$$U = 1$$
,  $V = 0$ ,  $\theta = 0$   
Outlet:  $\frac{\partial U}{\partial X} = 0$ ,  $V = 0$ ,  $\frac{\partial \theta}{\partial X} = 0$ 

All solid walls: U = 0, V = 0,  $\frac{\partial \Theta}{\partial N} = 0$ Heated wall: U = 0, V = 0,  $\Theta = 1$ 

In the above equations  $g\beta$ ,  $B_{\beta} \sigma \mu$  are the gravity acceleration, thermal expansion coefficient, Magnetic induction, electrical conductivity and dynamic viscosity of the fluid, respectively.

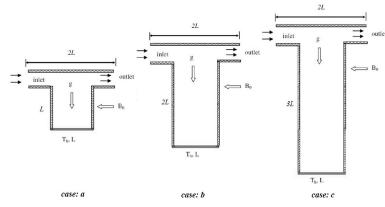


Figure 1: the 3 considered geometries and their boundary conditions

#### Solution procedure and validity

In this work the Control Volume method was applied to

discretize the dimensionless equations. Then the SIMPLE algorithm was used to solve the discretized equations. The convergence limit was set to:

$$|arphi^{m+1} - arphi^m| \le 10^{-6}$$

Where  $\varphi$  can be any general dependent variable. The result of the local Nu number of the geometry 1 are compared to the results of Rahman et al. [21] and shows a good agreement as can be seen in figure 2.

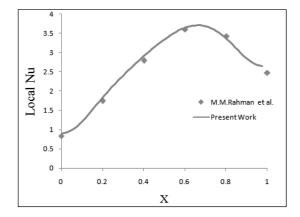


Figure 2: the local Nu number of the heated wall in geometry 1 compared to the results of [21]

#### **Results and discussion**

In this study, physical properties are constant and the

Re = 100, Ra =  $10^5$  for all cases and geometries. The Ha number is changed from 10 to 30 and the cavity depth for each case is defined as in the figure 1. The Pr number is also assumed to be fixed at 0.7 for 27°C.

Figure 3 shows the streamlines and isothermal lines for case *a* geometry (L\*L) for three different Ha numbers: 10, 20, 30. As it can be seen, in the case of Ha=10 the magnetic field do not influence greatly on the streamlines and as it is expected a clockwise vortex is formed. However, in the case of Ha=20 two main vortices are formed. This is due to the strength and direction of the magnetic field. This direction of magnetic field is

opposing the flow so in the case of Ha=30 the first vortex is almost vanished and the newly born vortex occupies the entire cavity.

Following the streamlines, the isothermal lines for this geometry change their shape by the increase of Ha. As can be seen the inclination of the isothermal lines in figure 3-a is to left. This can be assumed to be due to the moving direction of the flow but as the vortex direction is changed by the increase of Ha number, the inclination of the isothermal lines tends toward right (which is the new direction of the flow).

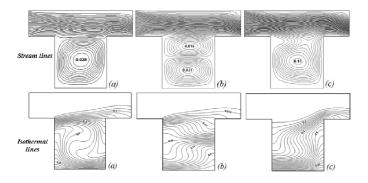


Figure 3: the stream lines and isothermal lines of the first geometry (case a) for *a*: Ha=10, *b*: Ha=20, *c*: Ha=30

As it is shown in figure 4, the main vortices of the cavity are weakening as the magnetic field intensity grows. It can be assume that the direction of magnetic field is opposing the entrance of flow in the cavity. This can lead to a weaker heat transfer rate due to the decrease of the convective heat transfer effect. This phenomenon can be observed on the isothermal lines as they grow and develop outward from case a to c (Ha=10 to 30) in this figure.

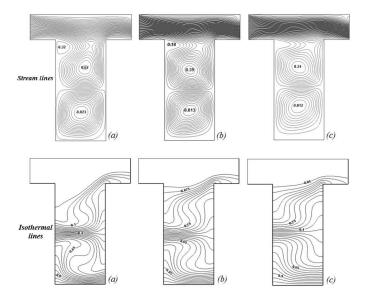


Figure 4: the stream lines and isothermal lines of the second geometry (case b) for *a*: Ha=10, *b*: Ha=20, *c*: Ha=30

In figure 5 the main 3 vortices are weakened as the magnetic field intensity and its representative Ha

number are increasing. One vortex is vanished while the other remaining two vortices are very weak. Also the small vortex in the top left corner vanishes as well. This can lead to a smooth long vortex with two cores which is developed from top to the bottom of the cavity.

Although the effect of the Ha increase in the geometry of 2L was not very suitable, here we can find it of some assistance. In this geometry 3 vortices are acting in Ha=10, 20. This can lead to a poor heat transfer rate so that its mean Nu number is less than other cases. But by increasing the Ha number the vortex is stretched from top to the bottom of the cavity. This phenomenon may increase the heat transfer rate. However, because of the weakening effect of the magnetic field, this vortex is not so strong and its Nu number cannot reach much higher than the other cases'.

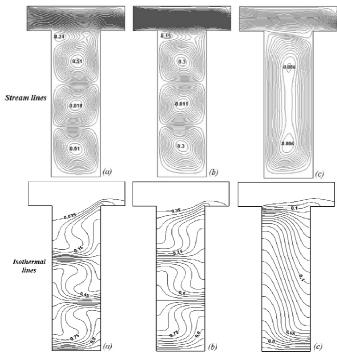


Figure 5: the stream lines and isothermal lines of the third geometry (case c) for *a*: Ha=10, *b*: Ha=20, *c*: Ha=30

Figure 6 presents the local Nusselt number of the bottom wall of the cavity for different Ha numbers on the considered geometries. The result shows that the maximum heat transfer rate for geometry a is for the case of Ha=30. As can be seen, the magnetic field has produced a stronger vortex than the other two Ha numbers. Also this vortex is in the direct contact of the free stream of the channel. In the case of Ha=20 one can observe the minimum heat transfer rate, it is due to the effect of the added vortex.

Case *b* of figure 6 shows a uniform decrease of the Nu number for increasing of the Ha number. But in case *c*, there is a change in Ha=30, as can be seen unlike the previous case in Ha=30 there is a slight increase in the convective heat transfer rate due to the reduction of vortices numbers.

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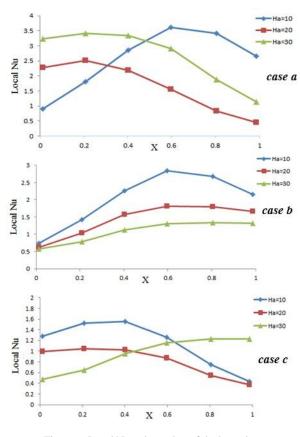


Figure 6: Local Nusselt number of the heated wall for the three geometries: case 1, case 2 and case 3

The mean Nusselt number of each case is demonstrated in figure 7-a. As can be seen, the highest Nu number is observed in the geometry of L\*L and Ha=30 and the minimum Nu number is in the geometry of 3L\*L and Ha=20. Also one can see that there is a relative minimum on the Nu plot for the cases of L\*L and 3L\*L while the case of 2L\*L experiences an absolute decrease of Nu by increasing Ha.

Figure 7-b demonstrates the temperature of the flow at the outlet boundary. It is seen that the outlet temperature for each Ha number directly follows the form of Nu plot. It shows that the conduction heat transfer can be neglected with respect to the convective form of heat transfer, which is expected.

Finally, the mean pressure change of the domain is demonstrated in figure 7-c. As it is seen that in the case of 2L\*L geometry the mean pressure gradient is higher than other cases but for Ha=30 it has a drastic decrease but the geometry of L\*L has a different style so that it has a sever increase at Ha=30.

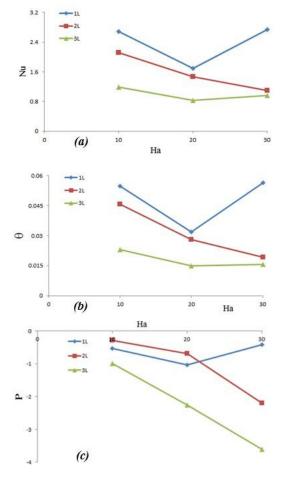


Figure 7: a) Mean Nusselt number of the heated wall for the three geometries b) The outlet temperature of the flow c) The mean pressure change in the domain.

### Conclusion

The Hydromagnetic fluid flow in a rectangular open cavity with variable depths has been investigated for 3 different geometries and 3 different Ha numbers. It was seen that the highest temperature gradient at the outlet boundary occurs in the case of geometry L\*L and Ha=30. This condition is also relevant for the highest Nu number on the heated wall. Also it was seen that the mean Nu numbers for the case of 2L\*L and 3L\*L at Ha=30 are almost the same so one can deduce that the change of cavity's depth at this Ha is effect less. Finally, a relative minimum is observed on the curve of Nu versus Ha for the L\*L and 3L\*L geometries while the case of 2L\*L experiences an absolute decrease of Nu by increasing Ha.

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