



Synthesis and gas permeation of polynorbornene by dinuclear α -diimine Ni-based catalysts: Experimental and quantum chemistry modeling

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Abstract

In this work, polynorbornene (PNB) was synthesized via dual-core catalyst successfully and applied in the gas membrane applications. The microstructure and physical properties of resultant PNB were evaluated precisely. FESEM images showed that PNB membrane had a dense and porous microstructure. XRD results indicated that polynorbornene had two sharp peaks at 2θ nearly 10° and 20° . The results of DSC analysis exhibited that with the design of the new synthetic system, the T_g reduced, though both molecular weight, and film-ability of polymer were improved significantly. A molecular weight of over 9×10^5 g/mol was obtained for PNB. The permeability values against CO_2 and CH_4 were 63.7 and 5.2 (Barrer), respectively, which were comparable with those of reported previously. Additionally, the obtained selectivity was 12.2. DFT-D simulation results showed that O_2 molecules have more tendencies to C_7H_{12} than that of other gas molecules and better capability to adsorb onto C_7H_{12} .

Keywords Polynorbornene · Dual-core catalyst · Glass transition temperature · Gas permeability · Membrane

Introduction

Norbornene and its derivatives are used in a wide variety of applications such as light-resistant materials, optical applications, electrical insulation, adhesives and rubbers [1–3]. These materials can be synthesized in two different ways, based on the desired properties in the final application [4, 5]. If the ring opening polymerization pathway is used, we will have rubber polynorbornene with unsaturated structures in the main chain. By contrast, in catalytic polymerization, we will have polynorbornene with the main chain structure of saturation that leads to the formation of both rigid mechanical properties along with high glass transition temperature (T_g) [6, 7]. These features endow polynorbornene as a fascinating candidate for gas separations applications. In this line, polynorbornene (PNB) synthesized by vinyl-addition (VA)

polymerization is a well-known candidate for this purpose [8–10].

Nevertheless, this kind of PNB has distinguished properties compared to conventional counterparts, synthesized by ring-opening metathesis polymerization, such as rigidity, bicyclic core of the norbornyl ring and the absence of any residual alkenes within the polymer backbone. These features give rise to the improvement of chemical stability in severe conditions like high thermal stability $>400^\circ\text{C}$, proper resistance against plasticization, resistance versus aging phenomena, promoting thermal transition temperatures, and the rise of free volume fraction in the solid-state polymer [11–14].

These outstanding properties are required for membrane-based applications that are faced with severe situations and huge amount of gas, for instance CO_2 separation from coal-fired power plants during post-combustion process [15], ion exchange membranes and fuel cell [16], CO_2 separation from natural gas, reverse osmosis process in the case of sea water desalination and separation of light hydrocarbons from natural petroleum gas [17–20].

Although great progress has been made in improving the properties of gas separation membranes in the last decade, there are still a number of weaknesses. These weaknesses

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have been mainly reported in the case of film-ability, brittleness of the prepared films and inferior elongation at break of samples [12, 21, 22].

According to literature survey, based on the published results, in most cases, polynorbornene and its derivatives synthesized by catalytic method (addition polymerization) possessed a higher permeability than polymers synthesized by ring opening method [12, 22, 23].

Some studies have also suggested that the catalytic system, besides increasing the molecular weight along with enhancing the physical and mechanical properties, will bring about a narrower molecular weight distribution compared to ring opening polymerization method [24]. In the case of catalytic systems, some studies have revealed that the active complex between nickel metal and the MAO co-catalyst is more stable than that of metal complexes such as palladium and titanium; hence can lead to higher molecular weight polymers [11, 25].

Recently, many studies have focused on the diimine nickel catalyst for the synthesis of aromatic and aliphatic olefinic monomers. All of the studies confirmed that these catalysts enhanced the catalyst properties including stability and activity in the comparison to the non-metallocene catalysts. It is worth mentioning that Peng and Chen [26] used diimine nickel catalyst for the polymerization and copolymerization processes of ethylene and some other aliphatic monomers. Moreover, these catalysts were successfully used for the synthesis of functional norbornene monomers in the studies of Wang et al. [27, 28].

Other researchers believe that the polymer microstructure is affected by the polymerization conditions and therefore different microstructures can be obtained by changing the reaction temperature, the type of solvent and the type of catalyst and co-catalyst [29, 30]. Zhao et al. have reported the preparation of a rigid random copolymer structure via nickel based catalyst in which the rotation around chain is difficult due to the spatial barrier made by the presence of the ring in the main chain [11]. In another study, nickel-catalyzed polynorbornene was introduced with an atactic structure in terms of ring placement in the chain structure.

Our studies showed that in the synthesis of this polymer, many research groups were encountered in several problems such as polymer insolubility, low molecular weight, and the lack of film formation due to the membrane fragility [31–33].

Regarding this fact, a dual-core catalyst was applied in this research so as to improve the physical–mechanical properties, film-ability of polynorbornene homopolymer as well as application in gas separation.

In spite of significant studies that have been carried out in the synthesis of polynorbornene and its derivatives for utilization in the membrane industry, the effect of dual-core catalysts on the properties of the synthesized polymer in the

application of gaseous membranes has not been investigated. Therefore, the present research aims to examine this issue.

In our previous work, the synthesis of linear polyolefins and relevant copolymers was reported for nickel-based dual-core catalysts, and consequently acceptable results were obtained for increasing molecular weight and final polymer properties [34–36]. The results of our previous study [37] showed the dinuclear α -diimine Ni-based catalysts was more active in comparison to mononuclear α -diimine for polynorbornene synthesis. So, the dinuclear α -diimine was used for the synthesis of polynorbornene. In this line, this new generation of catalyst is utilized in the case of polynorbornene homopolymer to tackle its drawbacks and improve gas separation properties. Besides, the density functional theory simulation (DFT) was performed to better exploit the adsorption of gas molecules via polynorbornene.

Simulation details

In order to evaluate the interaction mechanism between synthesized polymer and studied molecules, density functional theory (DFT) was used to gain more insights about the diffusivity of all gases into polynorbornene. All simulations were performed using the DMOL3 code of Materials Studio software by the Perdew-Burke-Ernzerhof (PBE) function at GGA level of theory. The electronic basis set used in this study was a double numerical plus polarization (DNP) set, which is the same as 6-31G** in Gaussian [38, 39]. In order to save time and cost in the simulation process, simplified models as the initial structure in DFT calculations must be considered. In this regard, a monomer of norbornene with a chemical formula C_7H_{12} was regarded for modeling of polymer. The adsorption energy of each cluster (E_{ads}) was determined via following formula:

$$E_{ads} = E_{complex} - E_{gas\ molecule} - E_{C_7H_{12}} \quad (1)$$

Where $E_{complex}$, $E_{gas\ molecule}$, $E_{C_7H_{12}}$ are the energy of the complex (gas molecule/monomer), gas molecule, and monomer, respectively, after geometry optimization. It has been reported that the interaction of gas molecules with norbornene monomer can be explained at the electronic level. Frontier molecular orbitals including HOMO and LUMO along with their relevant energies can be applied for evaluating the interaction process quantitatively. Consequently, the band gap of each isolated structure could be determined via HOMO (E_H) and LUMO (E_L) energies through the next formula:

$$\Delta E_{L-H} = E_L - E_H \quad (2)$$

According to the Eq. (2), one can predict the reactivity, stability, and the conductance of each molecule, or

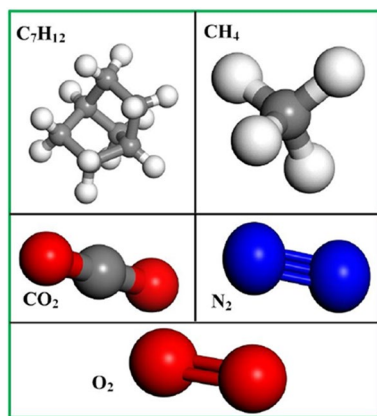


Fig. 1 Geometry optimized molecules via DFT at GGA/PBE level of theory

cluster. Figure 1 shows the optimized structures of defined molecules.

Experimental

Materials

All the manipulations of air/water-sensitive compounds were conducted under Ar/N₂ atmosphere using the standard Schlenk technique. All the solvents were purified prior to use. Toluene was purchased from the Mojallaly Co. (99.9%) was purified over sodium wire/benzophenone, and used as polymerization media. Dichloromethane (96%, Sigma-Aldrich Chemicals, Germany) as solvents were purified over calcium hydride powder and distilled prior to use in the synthesis of complex and ligand. Chlorobenzene was purchased from Merck Chemical Co. Norbornene monomer and modified methylaluminoxane (MMAO, 7% in toluene) were supplied by Sigma Aldrich Chemicals (Steinheim, Germany).

Ligands and complexes synthesis

The ligands and corresponding complexes were synthesized and fully described in our recent report [37] (Fig. 2).

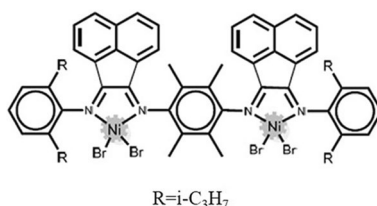


Fig. 2 Structure of dinuclear α -diimine Ni-based catalysts

Polymerization procedure

The synthesis approach of polynorbornene was performed based on our recently published paper [37]. The norbornene polymerization was carried out in a flask under Schlenk system. 7.52 g of norbornene, 16 ml toluene and MMAO 0.7% W/W solution in toluene were added in to the flask. Polymerization was started by adding catalyst in 2 ml dichloromethane. Reaction mixture was stirred at desired temperature for the required time. Reaction was quenched by adding acidified methanol. The precipitated polymer was filtered, washed with methanol for several times and then, dried in vacuum oven at 80 °C for 24 h.

Film formation

The preparations of films were obtained via casting of 5% of polymer solution (by weight) in trichlorobenzene. To begin with, 1 g polymer was dissolved in 30 ml of trichlorobenzene and was allowed to stir for 4 days before obtaining a clear solution. Afterwards, the resultant solution was poured into a 5 cm diameter petri dish to form a membrane. The petri dish was covered with an aluminum foil and transferred under the hood for 12 h and then transferred to a vacuum oven at 80 °C to increase the solvent separation rate. After 5 days, the dried membranes were placed in a water tank for 3 h and then separated from the petri dish and used for permeability testing. The thickness of the prepared films was 20–80 μm .

Characterization

The polymer molecular weight distribution (MWD) were determined with a high temperature gel permeation chromatography (GPC), run at 145 °C under a flow rate of 1,2,4-trichlorobenzene of 1 mL min⁻¹. The GPC was equipped with three detectors in series (infrared, light scattering, and differential viscometer) and calibrated with polystyrene narrow standards. The X-ray diffraction patterns were collected in transmission mode on a STOE Stadi P high-throughput powder diffraction apparatus equipped with a CuK α X-ray tube ($\lambda = 1.5418 \text{ \AA}$) and an image plate detector.

The morphological structure of both the surface and cross-section of the membranes was investigated by the field emission scanning electron microscope (FE-SEM, MIRA3 TESCAN, Czech Republic) operating at 10 kV acceleration voltage. Previously, the cross-section of the samples was prepared by fracturing in liquid nitrogen. The membrane surface and fractured surfaces were sputter-coated by a thin gold layer using a sputter coater (Q150R S, Quorum, England) during 60 s under 20 mA.

The permeability was studied by single-gas permeation using a constant-volume/variable-pressure apparatus. The

Table 1 The properties of synthesized polymer compared to literature

Polymer	catalyst	Al/Ni	M _n (kg/mol)	M _w (kg/mol)	PDI	Yield (%)	Ref
APN	NiBr ₂ [2,6-diisopropyl-C ₆ H ₂ -N=C-(C ₁₀ H ₆)-C=N-C ₆ H ₄ -N=C-(C ₁₀ H ₆)-C=N-2,6-diisopropyl-C ₆ H ₂]/MAO	1000	467	902	1.9	88	This work
APN	Ni(C ₆ F ₅) ₂ (SbPh ₃) ₂ /MAO	1000	84	277	3.3	58	[37]
APN	Ni(acac) ₂ /MAO	1000	388	730	1.9	72	[11]
APN	Ni(Nph) ₂ /MAO	1000	100	406	4.06	67	[19]
APN	[Ni(methallyl)Cl] ₂ /MAO	1000	142	366	2.58	83	[19]
APN	[Pd(allyl)Cl] ₂ /MAO	1000	285	661	2.32	82	[19]
APN	Ni(C ₆ F ₅) ₂ (SbPh ₃) ₂ /AgSbF ₆	2100	145	378	2.61	87	[19]

permeation cell was maintained at 28 ± 2 °C. The feed pressure was 1 ± 0.05 atm, on the permeate side of the film, the gas pressure was less than 10 Torr and considered negligible.

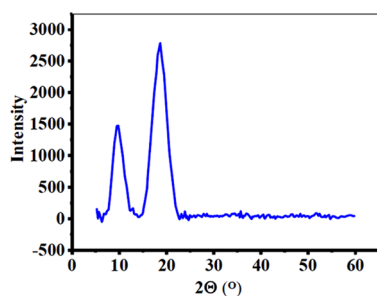
The membrane thickness was measured by a Mitutoyo Disk micrometer (369–511-30, ± 4 μm).

Result and discussion

The prepared films firstly characterized with different methods and secondly permeability of film tested for CO₂, CH₄, N₂, O₂ gases and compared with other researches in literatures and finally DFT-D simulation used for investigation of the adsorption of gas molecules via polynorbornene film.

Polymer characterization

Although the density of polynorbornene has been reported to be less than 1 g/cm³, some researchers believe that the higher density leads to the higher permeability [21], which can be more significant in the case of polynorbornene synthesized by the dual-core catalyst. As a result, a density of nearly 1 gr/cm³ was obtained in this study.

**Fig. 3** XRD pattern of polynorbornene

Molecular weight

As shown in Table 1, the use of dual-core catalysts allows the synthesis of polynorbornene with a molecular weight of over 9×10^5 g/mol that is soluble in such solvents such as chlorobenzene (trichlorobenzene) family and the possibility of dissolution; hence the chance of membrane preparation by casting method was enhanced. However, this polymer is still brittle compared to conventional polymers and needs further work to improve film-formation ability properties.

As shown in Table 1, synthesized polynorbornene using a nickel-based dual-core catalyst associated with a methylaluminumoxane cocatalyst had higher molecular weight and a narrow molecular weight distribution compared to similar studies reported by others.

X-ray diffraction pattern

The XRD diffraction pattern of synthesized polynorbornene is illustrated in Fig. 3. Polynorbornene possesses two broad peaks in the X-ray diffractometer plot, confirming the completely amorphous nature of this polymer. The peak observed at higher 2θ (20°) is related to intra segmental interactions and the peak observed at lower 2θ (10°) is ascribed to the inter segmental interactions. The crystallinity outcomes are summarized in Table 2.

Table 2 Crystalline properties of synthesized polynorbornene compared to reported data in the literature

Polynorbornene	2 θ [°]		Ref
	Low Angle	High Angle	
APN	10	18.5	[11]
APN	10	18.8	[37]
APN (R:-CH ₃)	9.5	18.2	[23]
APN	9.5	18.5	This work

The results are in agreement with those of previous reports [12, 21, 40] and confirm that, despite the significant increment in molecular weight, the possibility of crystal formation increased. However, the circular structures in the main chain are considered as a serious obstacle to the formation of crystalline structure in the polynorbornene family.

Based on XRD results, it can be concluded that small decrement in the diffraction angle further confirmed the positive influence of catalyst on the microstructure of polynorbornene. Besides, this decrease can be led to increasing of free volume and consequently better permeability.

Thermal analysis

Overall, there is no obvious relation between T_g and gas permeability properties. At temperatures below T_g , the main factor affecting the permeability properties is the free volume of polymer, which refers to its structure [22]. Note that T_g can be a sign of chain stiffness, and increases over the increasing of chain stiffness [29].

Nevertheless, some researchers have indicated that the permeability properties enhance upon improving of chain stiffness [21]. They believed that with increasing chain stiffness, the final density of the polymer increases and the increase in density improves the performance of permeability. Also, with increasing the chain stiffness, although the number of pores inside the polymer decreases, the size of this cavity increases. In other words, due to the difficulty of moving

and rotating the chain, changing the size of the pores is not possible. Consequently, the size of pores do not change during the function of the prepared membrane [23, 26]

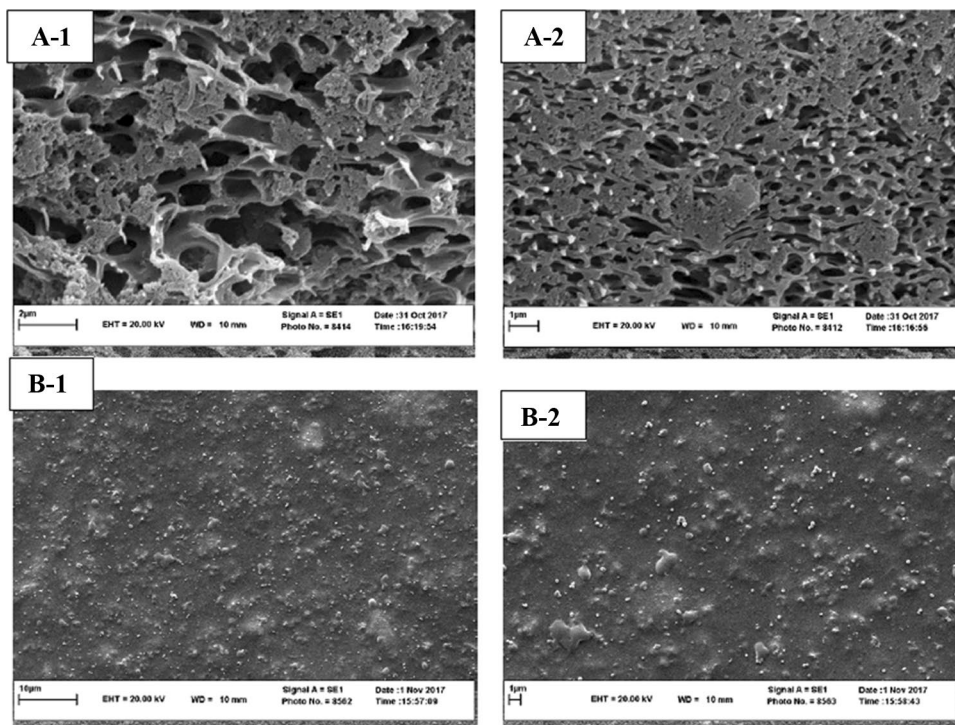
The results of DSC analysis showed that with the design of the new synthetic system, the T_g reduced but both molecular weight, and film-ability of polymer were improved significantly. Also the result of TGA test had been showed that the thermal stability of polynorbornene improved [37].

Field emission scanning electron microscopy (FESEM)

FESEM images of synthesized polynorbornene are illustrated in Fig. 4. As can be seen, a dense and porous microstructure is evident from FESEM micrographs.

This is due to the type of solvent used in the polymer film forming process. In fact, due to the high evaporation temperature of trichlorobenzene, longer time is required for the solvent evaporation process from the polymer structure. This is favorable for creating numerous pores within polymer film during slow removal of solvent. Additionally, the porous structure of film is desirable for permeability application. This behavior has been previously confirmed in the case of synthesized polymer in the presence nickel based catalyst compared to that of synthesized in the existence of palladium. In fact, the resultant morphology of synthesized polymer via nickel catalyst had smoother surface as well as a lot of pores [19].

Fig. 4 FESEM micrographs of **A** membrane surface and **B** cryo-fractured surface at different magnifications of **A-1** 2, **A-2** 1 μm , **B-1** 10 μm and **B-2** 1 μm



Permeability results

The free volume within the polymer structure plays the vital role in the permeability properties of glass polymers, but it should be noted that the family of polynorbornene and its derivatives do not have a high free volume and the relative free volume of this family is mainly reported between 9 and 16%. There is not much difference between the relative free volume between polymers synthesized by catalytic and ring-opening methods [13,17].

It seems that one of the reasons for the low free volume of the polynorbornene family is the lack of side chain in their structure and also the high stiffness of the polymer chain which has low mobility, and thus affects the free volume. This problem is also manifested in the density so that with increasing the stiffness of the chain, the density of the polymer increases and consequently the free volume of the polymer decrease [23].

Most of the researches on the membrane properties of polynorbornene and its derivatives have been stated that the permeability and selectivity of polynorbornene synthesized using the catalytic system were substantially more than those of polymer synthesized by ring opening method [12, 38, 39].

Sundell et al., have deduced that the effect of T_g reduction in the synthesized polynorbornene can be related to the decrease of kinetic resistance against the gas permeability. Therefore, it can be concluded that reducing the T_g of the synthesized polynorbornene in the present work from about 300 °C to around 240 °C, had a positive effect on the improvement of the permeability properties compared to similar studies. In fact, lowering the T_g leads to greater mobility of the chains and consequently enhancing gas permeability properties through the polymer [24].

As shown in Table 3, using dual-core catalysts, the solubility and film ability properties of polynorbornene membranes was improved. Moreover, a slight change in the free

volume structure along with increasing the distance between the chains was observed in which membrane has a quasi-dense structure on the one hand and a porous structure on the other, the rate of membrane permeability is close to that of methyl group structures in the lateral branch. As we know according to Robson trade off line for gas separation membranes it is expected that as the permeability of membrane increases, its selectivity decreases but as seen, the selectivity of the membrane was not changed much compared to similar samples in the literature [25, 40].

Aforementioned parameters may yield the improvement of permeability [4, 23]. However, in this study, we partially reduced this weakness in the polynorborn membrane with no side-chain by forming a membrane with variable porosity across the membrane.

The permeability values against CO₂ and CH₄

The research groups that have investigated the effect of the methyl side chain on the permeability properties of polynorbornene-based membranes, were looking for increasing the chain mobility by creating the side-chain within polymer, as well as increase the free volume and decrease the chain stiffness were 63.7 and 5.2 (Barrer), respectively, which are comparable with those of reported previously (Table 3). Additionally, the obtained selectivity was 12.2.

In fact, although obtained results of the permeability were lower than those of polynorbornene membranes having side groups [12], they revealed better results compared to many of the other studies performed on the polynorbornene.

Finally, the combination of the stability of chemical properties and permeability over time, as well as the acceptable permeability and selectivity in the class of glass polymers, making further research on this family of polyolefins can be attractive. Furthermore, there is a need for more attention to research and address the shortcomings of these polymers.

Table 3 Single Gas Permeability/Selectivity at 30 °C and 1 atm

Type of Polynorbornene	Permeability (Barrer ^a)				CO ₂ /CH ₄ Selectivity	Reference
	CO ₂	CH ₄	N ₂	O ₂		
APN-Ni(II)	63.7	5.2	3.5	O ₂	12.2	This work
Romp PN	15.4	2.5	1.5	16.3	6.16	[4]
APN- (R:-CH ₃)	396.3	30.3	24.1	2.8	13	[4]
APN- Ni(C ₆ F ₅) ₂ (SbPh ₃) ₂	28.2	2	1.9	89.2	14.1	[37]
APN- Ni[(Nph) ₂ Ni]-methylaluminoxane	33.6	2.6	1.5	-	12.9	[25]
APN-Ni(R:-CH ₃)	81.1	5.6	4.3	6.9	14.5	[23]
APN-Ni(acac) ₂	49.1	-	2.7	-	-	[11]
APN-Ni(C ₆ F ₅) ₂	52	3.1	2.5	10.8	16.7	[21]
ROMP-PNB(Catalyst Re)	23.6	4.7	2.2	11	5	[26]

^a 1 Barrer = 10⁻¹⁰ cm³ (STP) cm/cm² s cmHg

Table 4 The HOMO, LUMO energies (eV), and ΔE_{L-H} as the energy gap ($E_{LUMO} - E_{HOMO}$)

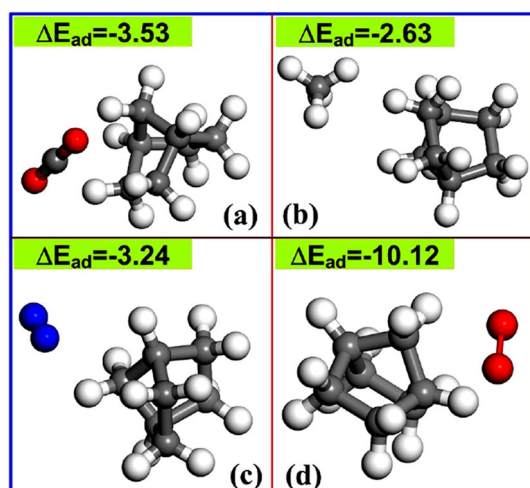
Molecule	E_H	E_L	ΔE_{L-H}	η
C_7H_{12}	-6.64	1.41	8.05	-4.025
CH_4	-9.27	2.82	12.09	-6.045
O_2	-5.81	3.83	9.64	-4.82
N_2	-9.96	-1.72	8.24	-4.12
CO_2	-8.95	-0.43	8.52	-4.26

Simulation results

The electronic properties of isolated molecules after optimization process are listed in Table 4. Overall, E_{HOMO} shows the capability of a molecule to donate electrons [41], while E_{LUMO} is a criteria regarding the ability of the molecule to receive electrons from other surface. As seen, the O_2 and N_2 had the highest and lowest HOMO energies, indicating the O_2 had the most favorable tendency to donate electron and N_2 showed the weakest trend.

Moreover, the highest value of the energy gap ΔE_{L-H} at 12.9 is ascribed to the CH_4 , suggesting its more stability compared with other structure. By contrast, C_7H_{12} experienced the lowest ΔE_{L-H} at 8.05, revealing its high reactivity, compared other molecules. As a result, a low value of the energy gap is a signature of a high reactivity for defines molecule, whereas high stability of the molecule is originated from high value in energy gap. Maroon and his coworkers have been shown similar results in polynorbornene derivatives for CO_2/N_2 separation [42].

The calculated adsorption energies of defined clusters after geometry optimization process values are illustrated in Fig. 5.

**Fig. 5** The final optimized geometries of **a** C_7H_{12}/CO_2 , **b** C_7H_{12}/CH_4 , **c** C_7H_{12}/N_2 , **d** C_7H_{12}/O_2 along with computed energy values**Table 5** The HOMO, LUMO energies (eV), ΔE_{L-H} as the energy gap ($E_{LUMO} - E_{HOMO}$), $\eta = 1/2 (\Delta E_{L-H})$ and the value of optimized energy of relevant clusters

Cluster	E_H	E_L	ΔE_{L-H}	η	E_{optm}
C_7H_{12}/CH_4	-6.59	1.29	7.88	3.94	-103.5
C_7H_{12}/O_2	-5.73	-5.72	0.01	0.005	-91.4
C_7H_{12}/N_2	-6.66	-1.78	4.88	2.44	-95.7
C_7H_{12}/CO_2	-6.68	-0.43	6.68	3.34	-104.1

The negative value of the adsorption energy for all clusters confirms the spontaneous adsorption process. In this case, the highest adsorption energy value was determined for C_7H_{12}/O_2 cluster, indicating it is the most stable cluster. In other words, O_2 molecules have more tendencies to C_7H_{12} than that of other gas molecules and better capability to adsorb onto C_7H_{12} . It can be attributed to the formation of stronger (shorter) intermolecular interaction between C_7H_{12} and O_2 compared to other complexes.

The electronic properties of optimized clusters at electronic scale, shown in Fig. 5, are summarized in Table 5.

According to the Table 5, it is evident that structures of C_7H_{12}/CH_4 and C_7H_{12}/O_2 had the highest and lowest ΔE_{L-H} , at 7.88, and 0.01 eV, respectively. It confirms that the C_7H_{12}/O_2 cluster saw the highest reactivity and stability compared to other samples. Nevertheless, the outcomes of optimized energy for each complex showed that the C_7H_{12}/CO_2 had the highest value, indicating the high stability of this cluster without considering the energy values of isolated molecules. The value of E_L for C_7H_{12}/CO_2 was -0.43 eV that is exactly the same as isolated CO_2 . It reveals that the electron acceptance capability of this cluster is originated from CO_2 molecules. The simulation results are in a fair agreement with experimental data. However, there is a little discrepancy between diffusivity data and adsorption energy obtained via DFT simulation. This can be ascribed to the consideration of only the monomer unit of polynorbornene that may restrict the calculation of appropriate chemical interactions (intra and inter molecular) involving between polymer and gas molecules.

Conclusion

In this research, a dual-core catalyst based on nickel associated with a methylaluminumoxane was applied to improve the physical-mechanical properties, film-ability of polynorbornene homopolymer as well as final application in gas separation. The synthesized polynorbornene using this dual-core catalyst had higher molecular weight (902 kg/mol) and a narrow molecular weight distribution (1.9) compared to similar studies reported by others. Furthermore,

such a molecular weight can be soluble in chlorobenzene (trichlorobenzene) solvent family; hence the chance of membrane preparation by casting method was improved. The appearance of two diffraction peaks at XRD pattern of polynorbornene at 2 θ : 10 and 20° confirmed its similar crystalline behavior compared to previously synthesized polynorbornene. A dense and porous microstructure is evident based on FESEM micrographs. It was due to the type of solvent used in the polymer film forming process. The permeability values against CO₂ and CH₄ were 63.7 and 5.2 (Barrer), respectively, which are comparable with those of reported previously. Additionally, the obtained selectivity was 12.2.

DFT-D simulation results showed that O₂ molecules have more tendencies to C₇H₁₂ than that of other gas molecules and better capability to adsorb onto C₇H₁₂.

In fact, obtained results of the permeability were lower than those of polynorbornene membranes having side groups; they revealed better results compared to many of the other studies performed on the polynorbornene. This can open new windows for researchers to design and synthesis polynorbornene with tunable microstructure and consequently excellent gas separation applications.

Declarations

Conflict of interest The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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