

# Gas Separation Performance of Polyvinyl Chloride Membrane

Mohammad Mohagheghian, Morteza Sadeghi, Mahdi Pourafshari Chenar and Mahdi Naghsh

Department of Chemical Engineering, Ferdowsi University of Mashhad, Mashhad, Iran  
mohammad\_2195@yahoo.com

Morteza Sadeghi

Department of Chemical Engineering, Isfahan University of Technology, Isfahan, Iran  
m-sadeghi@cc.iut.ac.ir

**Abstract**— The gas permeation properties of Polyvinyl Chloride (PVC) membrane was investigated for N<sub>2</sub>, O<sub>2</sub>, CH<sub>4</sub> and CO<sub>2</sub> gases. At 10 bar feed pressure and 25 °C the CO<sub>2</sub>/CH<sub>4</sub> and CO<sub>2</sub>/N<sub>2</sub> ideal selectivity of 40.36 and 20.18 was observed respectively. The effects of feed pressure and temperature on the permeation properties of polymer were studied. The permeability of gases was increased with increasing temperature and decreasing feed pressure. By using time lag method the diffusivity of gases through polymer has been calculated. Base on the solution diffusion mechanism the sorption constant of gases in polymer has been evaluated at different temperature and pressures.

## I. INTRODUCTION

Membranes have been successfully developed for gas separation. Separation of hydrocarbons from natural gas, nitrogen purification and the foremost CO<sub>2</sub> removal from natural gas are recognized as major established and high value industrial application of membrane. Recently polymeric membranes have attracted more attentions because of the low production cost and ease of processing, especially for hollow fiber preparation [1]. Glassy polymeric membranes are used for natural gas purification (CO<sub>2</sub>, H<sub>2</sub>O, H<sub>2</sub>S removal). The most common material used for such membranes is cellulose acetate. These materials only have CO<sub>2</sub>/CH<sub>4</sub> selectivities of 12–15 under typical operating conditions in the field [2], which is well below the low-pressure mixed gas selectivity of ~30 for cellulose acetate dense membranes with zero permeate pressure [3]. The decline in selectivity is primarily due to swelling-induced plasticization of the membrane by CO<sub>2</sub> and heavy hydrocarbons. The development of stable membrane materials with CO<sub>2</sub>/CH<sub>4</sub> selectivities of 40 would significantly enhance the competitive position of membranes relative to alternate technologies such as amine scrubbing [2]. PVC is a glassy polymer with high mechanical strength, high thermal stability. This polymer is available with low cost. In this paper the Gas Separation Performance of Polyvinyl Chloride Membrane was studied.

## II. EXPERIMENTAL

### A. Materials

PVC powder was procured from Vinythai Co, Thailand. (K-Value = 65-67, Specific Viscosity = 0.36-0.38) Dimethylformamide (DMF) solvent was purchased from Merck. The CO<sub>2</sub>, O<sub>2</sub> and N<sub>2</sub> gases (purity 99.99) were

purchased from Ardestan Gas Co., Iran and also CH<sub>4</sub> (purity 99.95) was purchased from Technical gas service.

### B. Dense Membrane Formation

A solution casting method was used to prepare the dense film [4]. The average thickness of the films was 35 microns.

### C. Gas Permeation Tests

The gas permeation properties of membranes were specified by a variable pressure/constant volume method [5]. The gas permeability was determine at 6, 8, 10 bar pressure and at 25°C and 35 °C. The test cell area was 13.2 cm<sup>2</sup> and the leak rate was 10<sup>-5</sup> mbar/s, indicated a negligible effect on permeability data. The rate of pressure increase (dp/dt) (mbar/s) at steady state was used for the calculation of gas permeability with the following equation:

$$P = \frac{273.15 \times 10^{10} V l}{76 A T (p_2 - p_1)} \left( \frac{dp}{dt} \right)$$

where P is the gas permeability of a membrane in Barrer (1 Barrer = 1 × 10<sup>10</sup> cm<sup>3</sup> (STP).cm/cm<sup>2</sup> s cmHg), V is the volume of the down-stream (cm<sup>3</sup>), A refers to effective area of the membrane (cm<sup>2</sup>), l is the membrane thickness (cm), T is the operating temperature (K) and finally p<sub>2</sub> and p<sub>1</sub> (mbar) are pressure of the feed gas in up-stream and down stream respectively.

## III. RESULTS AND DISCUSSION

### A. Pure Gas permeation

The pure gas N<sub>2</sub>, O<sub>2</sub>, CH<sub>4</sub> & CO<sub>2</sub> permeabilities (P) and diffusion coefficients (D) were determined simultaneously by recording the increase of downstream pressure with time and solubility coefficients (S) were estimated as S = P/D. Tables 1 & 2 shows the Permeability, diffusivity and solubility coefficient of PVC membrane at 10 bar at 25°C and 35 °C respectively. In Tables 3&4 same properties were reported at 8 bar and 6 bar feed pressure respectively.